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Comparative Investigation of Thermodynamic Parameters of Seafood Waste as an Inhibitor for Mild Steel Corrosion in Varied Acidic Concentration

M. PRIYA^{1*}, M. SENTHIL², S. KALAI SELVI³ and S. RANJITHA⁴

 *1.3Department of Chemistry, Velalar College of Engineering and Technology (Autonomous), Erode–638 012, Tamilnadu, India.
 ²Department of Chemistry, Kandaswami Kandar's College, Periyar University, Velur-638 182, Tamilnadu, India.
 ⁴S.Ranjitha, Department of Physics, Velalar College of Engineering and Technology (Autonomous), Erode-638 012, Tamilnadu, India.
 *Correspnding author E-mail: phddatas15@gmail.com

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ABSTRACT

Mild steel (MS) is the material that is frequently used in various sectors because of its specific properties like ductility and malleability, however it corrodes readily when exposed to corrosive environments. Inhibition is the best method to prevent corrosion, since it may be adjusted or added in place without interrupting a process. The present study focused on the thermal behavior of Crab Shell extract (CSE) as corrosion inhibitor on the surface of the MS in 0.5M and 1M sulphuric acid medium. Temperature study was employed to test the inhibitory action of the extract on MS using weight loss measurement. The effectiveness of inhibition declines with the rise of temperature. In 0.5M $_2SO_4$ at 303 K, the maximum efficiency was observed. The nature of adsorption in both the acidic medium follows El-Awady adsorption isotherm. The activation and thermodynamic study revealed that the reaction is spontaneous in nature. The inhibition process is endothermic which is confirmed by the positive enthalpy values.

Keywords: Corrosion, Crab shell, Mild steel, Temperature, Adsorption.

INTRODUCTION

In modern industry, sulphuric acid is a commodity chemical and is used for the manufacturing of variety of products like automobile batteries, fertilizers, sulphonation agents etc., and also it is used as pickling agent to remove the surface impurities from metals and alloys. Mild steel is an in-demand material in the past few years due to its qualities such as ductility, weldability, malleability, machinability etc.,^{1,2} It is a cost-effective type of steel, which many industrialists prefer for their industrial projects. However, it is very sensitive towards acid, alkali and in salt solution. It will rust over time unless it is treated with some sort of protective coating to prevent corrosion. Synthetic inhibitors which is used initially for corrosion protection have some negative impact like toxicity and high cost.³ Researchers

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focused on green inhibitors because of its abundance, environmental safety and low cost. Sea food waste is the most abundant one which causes harmful impact on environment if it is not properly disposed. Crab shell consists of calcium carbonate, protein, chitin and carotenoids. In view of these points, the current research focuses on employing crab shell as an inhibitory source to protect mild steel from corrosion in two different sulphuric acid media. Based on the literature review, 0.5M and 1M concentration sulphuric acid is used for the investigation.

EXPERIMENTAL MATERIALS AND METHODS

Preparation of test specimen and inhibitor

5x1 cm² size MS specimens were polished mechanically with emery paper followed by the process of degreasing and then washed with deionized water. The dried samples were stored in a desiccator and used for the experimental procedure. Crab shells were collected from fish market. It is washed with plenty of water and shadow dried. The dried shells were crushed using a mortar. Refluxing 25 g of powdered crab shell for 3 h with 500 mL of 0.5M H₂SO₄ and the solution was cooled overnight. It was then filtered and made up to 500 mL to get 5% extract. From the stock solution, various inhibitor concentrations were prepared.

Weight loss measurements

Weight loss was measured at four different temperature (303K, 313K, 323K & 333K) after 3 h of immersion period. Pre-weighed MS specimens were immersed in 100 mL of $0.5M H_2SO_4$ in absence and presence of inhibitor (0.1% to 0.5%) and placed in a thermostat for 3 h at a specific temperature. After the elapsed time, the samples were removed, washed with deionized water and then with acetone. Accurate reweighing was done on the air-dried samples. Triplicate measurements were performed at all the temperatures.

The percentage of inhibition efficiency (η) and surface area coverage (Θ) were calculated using the following formulae 1&2⁴

 $\eta(\%) = (w_0 - w_i) / w_0 \times 100$ (1)

 $\Theta = (w_0 - w_i) / w_0 \tag{2}$

Where, w_0 and w_1 is the weight loss values without and with inhibitor and Θ is the surface coverage of specimen by the inhibitor.

Adsorption isotherms

Adsorption investigations provide insight into the character of adsorption of inhibitor on metal surfaces. Several adsorption isotherms can be employed to find out the type of interaction between metal surface and the inhibitor. In order to find out the best fit, El-Awady (modified Langmuir adsorption), Freundlich and Temkin adsorption isotherms were plotted based on the following expressions in linear forms given in 3,4 & 5 respectively.⁵

El-Awady: $\log \Theta/(1-\Theta) = y \log C_{B} + \log K$ (3)

Freundlich:
$$\log \Theta = \log K_{ads} + n \log C_{R}$$
 (4)

$$Temkin: \Theta = InC_{R} + K_{ads}$$
(5)

Kinetic and thermodynamic parameters

Energy of activation, entropy and enthalpy values were calculated using Arrhenius equation and Transition state equation 6 & 7

$$\log C_R = \log A - \frac{E_a}{2.303RT} \tag{6}$$

$$\log \frac{CR}{T} = \left[\log \left(\frac{R}{Nh} \right) + \left(\frac{\Delta S}{2.303R} \right) \right] - \frac{\Delta H}{2.303RT}$$
(7)

Where, C_{R} -corrosion rate, A-Arrhenius preexponential factor, Ea-activation energy, R-universal gas constant, T-temperature, N-Avogadro number, h-Planck's constant, Δ S-entropy of activation and Δ H-enthalpy change.

From the graph of the transition state equation, the enthalpy change and the entropy change was evaluated from the slope (- Δ H/2.303R) and the intercept (log(R/Nh)+(Δ S/2.303R) respectively.⁶

The most important thermodynamic adsorption parameter ΔG was calculated by the following equation 8.

$$\Delta G_{ads} = -RT \ln(55.5 \text{ K}_{ads}) \tag{8}$$

Where, Δ G-free energy of adsorption, K-adsorption equilibrium constant, R-gas constant, T-absolute temperature and 55.5-concentration of water in solution (molL⁻¹)

RESULTS AND DISCUSSION

Effect of temperature

The efficiency of the inhibitory action of usually has a close relationship with its concentration and the environmental temperature.⁷ The graphical representation of the temperature study was given in Fig. 1. Effect of temperature with various concentration of inhibitor in 0.5M and 1M acidic media are listed in

Table 1. In both the concentration of acidic medium, the effectiveness of inhibition process decreases at subsequent higher temperatures, which means that there is an acceleration of desorption rate rather than adsorption at elevated temperature.⁸ The maximum efficiency was recorded with optimum concentration of 0.5% CSE at 303K in 0.5M sulphuric acid. Surface coverage is comparatively higher in 0.5M when compared to 1M solution.

Concentration of acid Concentration of inhibitor (%)							
		0001	01010	02010	0001		
0.5M H ₂ SO	Blank	-	-	-	-		
2 4	0.1	71.69	44.92	24.20	17.77		
	0.2	75.80	60.16	46.27	19.70		
	0.3	78.54	70.70	60.64	44.35		
	0.4	81.28	75.78	66.49	51.38		
	0.5	83.56	80.08	72.34	55.79		
1M H _s SO	Blank	-	-	-	-		
2 4	0.1	60.37	21.44	20.78	10.14		
	0.2	69.31	45.58	40.03	26.60		
	0.3	75.78	63.41	57.35	36.76		
	0.4	79.13	68.88	62.81	49.69		
	0.5	81.37	74.68	69.87	53.87		
80 - 70 - 60 - 50 - 20 - 20 - 20 -		80 0 10 - 0 - 0 - 0 - 0 - 0 - 0 - 0 - 0		- 303K - 303K			
0.1 0.1	2 0.3 0.4 0.5	0.1	0.2 0.	3 0.4	0.5		
Con	centration of Inhibitor (%)	Concentration of Inhibitor (%)					
	(a)	(b)					

Table 1: Influence of temperature on inhibition efficiency

Fig. 1. Influence of temperature on inhibition efficiency in (a) 0.5M and (b) 1M H_2SO_4

Adsorption isotherms

The nature of adsorption of inhibitor on MS surface can be predicted by the adsorption isotherms. In the present study, the three adsorption isotherms viz., El-Awady, Freundlich and Temkin adsorption isotherms were tried to find the best adsorption isotherm. Linear regression co-efficient values obtained from the plots of El-Awady, Freundlich and Temkin adsorption isotherms were found to be close to unity in both the concentrations. Comparatively higher R² values found for El-Awady adsorption isotherm and the values were displayed in Table 2 which predicts the

Table 2: R ² values of El-Awady				
adsorption isotherm				

formation monolayer adsorption on MS surface9 and

El-Awady isotherm was shown in Figure 2.

Temperature (K)	R ² Values				
	$0.5MH_2SO_4$	$1MH_2SO_4$			
303	0.9569	0.9909			
313	0.9969	0.9875			
323	0.9945	0.9919			
333	0.9950	0.9904			



Fig. 2. El-Awady adsorption isotherm for CSE in (a) 0.5M and (b) 1M H₂SO₄

Activation parameters

The Arrhenius and transition plot of inhibition process on MS in 0.5M and $1M H_2SO_4$ is shown in Fig. 3 and 4 respectively. Activation energy values, enthalpy and entropy values were determined and presented in Table 3. The activation energy values were higher in presence of CSE when compared with the absence of CSE for both the concentration leading to the conclusion that the inhibitor adsorbed on the surface of the MS was due to the increased energy

barrier. Activation energy values less than 80KJ/ mol suggests the process physical adsorption.^{10,11} Enthalpy reading that are positive predicts that the dissolution of metal is endothermic and the spontaneity of the adsorption process is indicated by the negative free energy values. The negative entropy values infers that the activated complex in the rate deciding step represents an association rather than detachment step, meaning that a diminish in disordering takes place on going from reactant to activated complex.^{12,13}

Conc. of acid	Conc. of inhibitor (%)	Ea (kJ/mol)	303K	-ΔG (KJ/mol) 313K	323K	333K	ΔH* (kJ/mol)	-∆S* (J/mol)
0.5M H ₂ SO ₄	Blank 0.1 0.2 0.3 0.4 0.5 Blank 0.1 0.2 0.3 0.4 0.5	33.11 62.92 66.60 61.66 62.23 63.75 42.58 63.07 65.14 67.79 66.01 66.64	- 18.24 17.03 16.40 16.10 15.94 - 16.96 16.20 16.00 15.76 15.39	- 15.89 15.69 15.85 15.78 15.85 - 13.04 14.16 14.99 14.88 15.05	- 13.88 14.16 13.99 13.85 13.78 - 13.35 14.00 14.79 14.63 14.88	- 13.23 11.66 13.80 13.78 13.66 - 11.43 12.74 12.93 13.60 13.44	13.23 25.94 27.61 25.48 25.74 26.41 39.96 60.45 62.53 65.17 63.39 64.02	192.65 188.09 187.53 188.44 188.41 188.21 190.41 187.20 186.98 186.66 187.03 186.99
2.8 2.6 2.4 2.2 0 0 2.0 1.8 1.6 1.4 3.00	 B 0.1% 0.2% 0.3% 0.4% 0.5% 3.05 3.10 3.15 1000/T (K (a) 	• • • • • • •	3.30	0.4 0.2 0.0 -0.2 -0.2 -0.4 -0.6 -0.6 -0.8 -1.0 -1.2 -3	■ B ● 0.1 ● 0.2 ● 0.3 ● 0.4 ● 0.5 ● 0.4 ● 0.5 ● 0.4 ● 0.5 ● 0.5 ● 0.4 ● 0.5 ● 0.4 ● 0.5 ● 0	3.10 (t	3.15 3.20 00/T (K ⁻¹)	3.25 3.30

Table 3: Kinetic and thermodynamic parameters of adsorption of CSE

Fig. 3. (a) Arrhenius and (b) Transition plot for CSE in 0.5M H₂SO₄



Fig. 4. (a) Arrhenius and (b) Transition plot for CSE in 1M H₂SO₄

Suggested Mechanism of inhibition

Organic compounds containing hetero atoms with π bonds could act as an efficient inhibitor against corrosion. Crab shell used for the present study, are rich in calcium carbonate and protein. Calcium carbonate and other minerals were removed as residue during demineralization process. The protein content was hydrolysed as amino acid that consists of amino and carboxylic acid group and retain in the extract. The hetero atoms present in amino acid is responsible for the corrosion protection.¹⁴

CONCLUSION

Based on the results of the current work, the following conclusions were drawn:

CSE has a significant inhibitory effect on the surface of the MS in both 0.5M and 1M H_2SO_4 . The efficiency of the inhibition declines with increase in temperature. The rate of

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adsorption is little bit higher in $0.5M H_2SO_4$ when compared to $1M H_2SO_4$. Linear regression coefficient values of modified Langmuir adsorption isotherm were found to close to unity which supports the formation of monolayer on metal surface. Increased activation energy confirmed the process of adsorption of inhibitor in both the acidic medium. Positive enthalpy values and negative free energy values indicate the endothermic and spontaneous nature of the adsorption process, respectively, and inhibitors adsorb onto the metal surface through physical adsorption.

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Conflict of interest

The authors affirm that there is no conflict of interest.

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