



Novel Integrated Ultrafiltration and Reverse Osmosis System in High Quality Drinking water Production

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ABSTRACT

Modernization in water technology plays a major role in ensuring a clean, safe, and feasible supply of drinking water. Enhancing performance in terms of price and quality, flow ability of the plant, sustainable development; integrated membrane processes have been developed. The most crucial issues found in RO applications such as concentration polarization and membranes fouling are reduced by using this integration of membranes. Conventional reverse osmosis filtration has sand and coke filters as pre filters. In this work these pre filters have been replaced by ultra-filtration which ensures undoubtedly the best quality of water despite the quality of feed with low power consumption and chemicals. These integrated systems are the better thing for complete elimination of microorganism and water contaminants in their category of selection. The present work also contributes on water quality analysis for brackish water using both the above desalination membrane technology. This integrated system can be remotely monitored and self-adapted model-based control.

Keywords: Reverse osmosis, Ultra filtration, Desalination membrane technology, Membrane fouling, Integrated system, Pre filters.

INTRODUCTION

The scarcity of potable water poses a big problem where freshwater is becoming very scarce and expensive.¹ One of the major international health issues in today's scenario is clean drinking water. Nearly 25 percent of global world has no access for fresh water². All the parts of world found to have abundant fresh water and the main issue is all these waters are polluted either directly or indirectly by natural sources or manmade activity. Revolution in modernization and development in industries and their machinery operation need clean water for their

process. Thus the demand for the clean water is magnificently expanded more and made the current scenario scarce. As a result, water consumption –related deaths in the earth are currently a major possible cause of mortality. It is more alarming issue in this existing situation consuming polluted water and death rate due to water contamination³.

One of the development in which required membrane purifying water that uses the reverse osmosis membrane is progressively transferred via the solvent (typically water) is reverse osmosis⁴. Pressure act as a hub for resolving water hydrostatic



gradient. Integrated membrane module may be severely affected by RO Membrane pore size, concentration factors, membrane roughness, chemical stability and other factors, such as fouling, scaling and premature membrane deterioration. This can result in reduced of flux, lesser rejection rate higher pressure drops, shorter membrane life and high operating costs. Ultrafiltration (UF) is tested to be competitive compared to standard treatments. UF is used to supplement the approval process, i.e; co-precipitation, sedimentation and filtration, in standard desalination plants and can be described as the clarification and disinfection of the membrane activity. UF membranes are normally permeable and all impurities microbes, particularly macromolecules, such as microorganisms are refused. Compared to other traditional clarification and disinfection (post chlorination) methods, the primary characteristics of low pressure UF membrane processes are the necessity of negligible chemicals, girth filtration as opposed to media depth filtration, strong and constant consistency of treated water in terms of particle and microorganism reduction regardless of water quality process and plate filtration. Source quality of water greatly impacts UF membrane performance. In an external flow configuration with a relatively modest pore diameter, ultra filtration PVDF flat sheet membrane make it a great choice to safeguard all downstream such as reverse osmosis. With an industry leading ultra filtration membrane region of low energy and chemical utilization, the modules retain the optimum showing, accurately reducing the amount of configuration for the design. The pore size range between 0.01 to 0.1 μm , the pore sizes of ultra filtration membrane pore size fall between that of nanofiltration and microfiltration. The main advantage of UF is that specified given trans-membrane pressure, the membrane flux is much greater for UF than RO. The energy required is less for specified flow rate of UF membrane than to RO membrane of same surface area. For low pressure application, UF has made us apractical alternative. The success of membrane lies in the following pre-treatment processes(1) Application areas influence desalination of seawater, treatment of wastewater, separation in the biotechnology and food industries and chemical production.

MATERIALS AND METHODS

Collection of Samples: The water sample from different parts of Chennai were collected and classified based on TDS of water sample.

Physico-chemical Analysis

The collected water samples were tested by using physical and chemical analysis method. The physical analysis includes the determination of Total suspended solids, Total dissolved solids, PH, conductivity, salinity, turbidity and the chemical analysis are shown below:

Estimation of Suspended Solids (Non-Filterable Solids)

The Cauldron is washed with a filter paper that is ignited in the oven at a watch glass (W1). Then the sample weighs 25 mL and via the cauldron, filtered. The dried crucible is kept at 103°C for 24 h, allowed to cool in the desiccators and weighed (W2). The value of the suspended solids is calculated as follows:

$$TSS = \frac{W2 - W1}{V} \times 100 \text{ mg/ml}$$

Where : W1 = Weight of empty cauldron along with filter paper in mg

W2 = Weight of the cauldron in addition with filter paper after drying in mg

V = Volume of the sample taken in mL.

Estimation of Total dissolved solids

Total dissolved solid was evaluated by simple method based on evaporating the water samples to dryness. The 50 mL of given sample were taken in evaporating dish by heating for drying at 180°C to a constant mass for 1 to 2 hours. Total dissolved solids were calculated as follows:

$$TDS = \frac{\text{mg of residue}}{\text{ml of sample}} \times 1000$$

Estimation of pH of the water sample

The pH of the sample is measured by the theory of ionization of water due to formation of hydrogen ion (H^+) and hydroxyl ion (OH^-). The pH scale is used to calculate the pH of the medium, i.e. the acidity or alkalinity of the medium. The pH meter is set to level surface. The electrode calibration was done using the suitable buffer solution. After calibration, the pH meter, the electrode is washed by dipping

into deionised water to remove any adhering buffer. The sample solution is collected and the electrode is immersed in it and its reading is noted. Once again pH of the sample is measured by washing the electrode by dipping it in distilled water.

EXPERIMENTAL

The sample water treatment process in this system includes following phases. During the first phase, the sample ground water passes through a sediment filter. All of the pollutants and retained solid are removed in this first stage. Then water sample send to UF membrane chamber where the removal of macromolecules of the given treated water sample. Then this sample is sent to main chamber where the water is passed through a semi permeable filter at pressure of 30-40psi thus the RO purification process is done. The suspended impurities including lead, pesticides, sulphates and nitrates, passes with a very narrow pore diameter of 0.01micron. The final chamber process uses UV lamp pf 11 watts to put the water UV filtration. The water is made of free of germs and safe for drinking by removing all microorganism. The advantage of ultraviolet rays, extremely deadly to microorganism, is that attack them completely so that they cannot replicate. This process is more unique that without addition of any chemicals, 99.9% of all microorganisms are killed. Finally the treated water is collected in pure water tank.

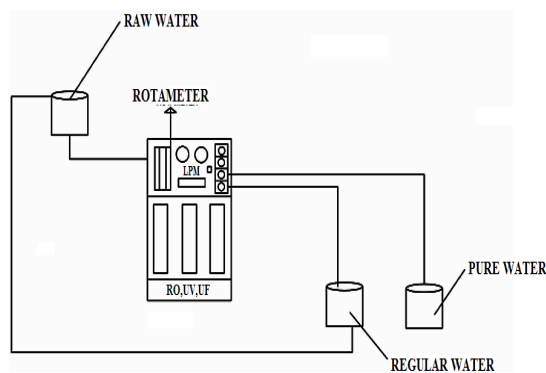


Fig. 1. Experimental set up (RO-UF set up)

RESULTS

The collected water samples were tested by using physical and chemical analysis method. The physical analysis includes the determination of Total suspended Solids, Total dissolved solids, pH, conductivity, salinity, turbidity and odour are shown

in Table 1. The collected water samples were tested by using chemical analysis method. The chemical analysis values for raw water samples are shown in Table 2.

Table 1: Physical Analysis of water

Parameter	Raw water samples at room temperature		
Samples	1	2	3
Total dissolved solids ppm	500	1000	1500
Total suspended solids	3	4	8
pH value at 25°C	6.81	6.71	7.23
Conductivity	1250	1460	1700
Salinity ppm	450	730	810
Odour	NIL	NIL	NIL
Turbidity (NTU)A	1	1	1

Table 2: Chemical Analysis of water

Parameter	Raw Water Samples at Room Temperature		
Samples	1	2	3
Total Hardness as CaCO ₃	320	421	541
Calcium Hardness as CaCO ₃	251	327	421
Chlorides as Cl	250	451	1100
Sulfates as SO ₄	280	320	540
Total Iron as Fe	0.31	0.42	0.48
Calcium as Ca	104	202	284
Magnesium as Mg	21	45	49
Manganese (mg/L)	0.1	0.12	0.15
Zinc	1.0	1.0	1.0
COD	3	2.4	2.1

DISCUSSIONS

The ultra filtration process is the solution separation process in which there is the variation in pressure between two sides of the membrane as the guiding factor, and the mechanical separation⁵. The pore size of sieve is 0.01-0.1µm.⁶ UF may remove particles such as colloidal particle, bacteria, virus, macromolecule organics, etc., but it may not reduce low molecular organics or ionic pollutants⁷. Based on total dissolved solids of samples, other physical parameters are varying. Permeate volume and permeate flux has been given in Table 4. Individual treatment with UF membrane and integration membrane has been given separately in Table 5.

Table 3: Specifications of Integrated portable UF and RO system

Specifications	Ultra filtration	Reverse osmosis
Material	Hollow fiber	PTFE
Flow	500litres /hr	500 litres/h
Automation	automatic	Automatic
Pore size	0.1 microns	0.0001 microns

Table 4: Permeate Volume & Permeate Flux

Time (min)	Permeate Volume (mL)			Permeate Flux $\times 10^{-3}$ l/m ² h		
	1	2	3	1	2	3
1	65	80	82	0.8	0.82	0.84
2	140	142	148	0.76	0.77	0.79
3	200	210	215	0.74	0.75	0.76
4	240	268	280	0.72	0.73	0.75
5	343	358	395	0.72	0.72	0.73
6	425	480	490	0.72	0.72	0.73
7	485	490	495	0.72	0.73	0.74
8	520	540	555	0.71	0.72	0.74
9	624	680	710	0.71	0.71	0.72

The parameter like pH, conductivity, salinity increases with increase in Total dissolved solids

from data observation higher the Total dissolved solids of water, higher the electrical conductivity of water sample⁹. The carbonate, bicarbonate and CO₂ concentration as a part of Total dissolved solids can affect on the values of pH. The total dissolved solids concentration is the total charged ions present in the water sample (sum of cations and anions)⁹. The conductivity increases as salinity increases because of the conduction of electric current due to dissolved salts and other inorganic chemicals. Permeate volume increases with increase in time shown in Fig. 2. Permeate flux decreases slowly with time shown in Fig. 3, with the increase in the concentration. In constant concentration case complete reuse of permeate and retentate is maintained. The ultra filtration membrane has remarkable role on removal of iron. The water present in the iron is in the form of flocs or complexes and few of iron are in Free State. Small molecule organic contaminants are not removed by ultra filtration¹⁰, experiments show that ultra filtration does not have separation effect on COD and Mn.

Table 5: After Treatment with Ultra filtration and Reverse osmosis

Samples	After UF treatment after			Treatment with integrated UF, RO, UV		
	1	2	3	1	2	3
Total Hardness as CaCO ₃	320	421	541	9.0	9.5	9.8
Turbidity	0.5	0.5	0.5	2	3	4
Total hardness	250	300	320	122	124	136
Sulfates as SO ₄	180	220	240	10	12	13
Total Iron as Fe	0.10	0.11	0.13	0.1	0.1	0.1
Calcium as Ca	100	102	184	52	56	58
Magnesium as Mg	21	45	49	10	12	14
Manganese (mg/L)	0.09	0.1	0.15	0.01	0.02	0.03
Zinc	0.9	1.0	1.0	1	1	1
COD	2.8	2.4	2.1	1	1	1
TDS	400	890	1260	82	88	92

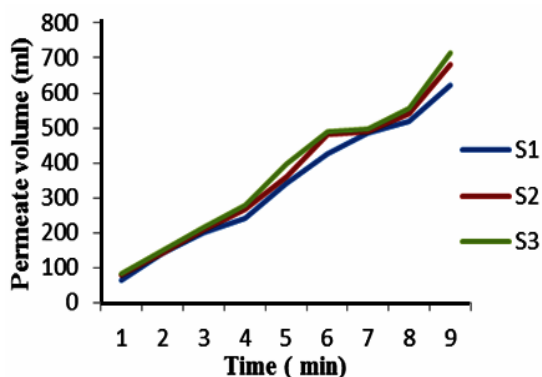


Fig. 2. Permeate volume vs Time of different samples water

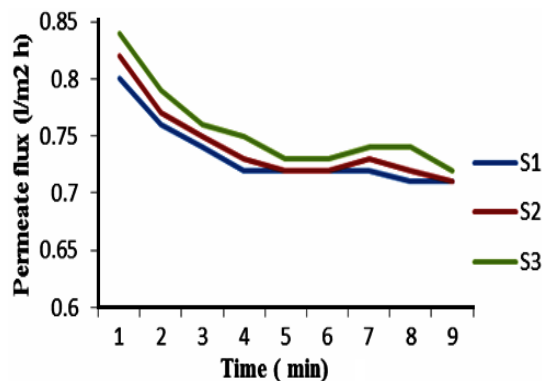


Fig. 3. Permeate flux vs Time of different sample water

CONCLUSION

This integrated system is a great choice for virus, pathogens, dissolved particles, colloidal particles and water contaminants to be highly removable. Ultrafiltration (UF) has been shown to be efficient in treatment compared with traditional treatment. UF is used to remove the clarification step in conventional RO water treatment plant. Ultra filtrate water is effectively free of particles, colloidal particle and dissolved solids. Therefore, slotting of RO feed channels is reduced and the RO cleaning intensity can be notably minimized with this integration method. The operating pressure decreases with rate of removal of most pollutants and increases with system membrane flux. The integrated system (UF-RO combined process) observation shows that the dual-membrane process is an excellent option

for the water treatment purifying process, with the efficiency of low water efficiency standards, superior water value, high recovery etc. The RO membrane effectively discards pollutants and maintains a sufficient sum of life saving elements, meeting norms for high quality potable water thus, the UF-RO integrated combined process is best suited for the design of direct drinking water system.

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Conflicts of interest

The authors declare no conflicts of interest.

REFERENCES

1. Majlinda Daci-Ajvaz.; Bashkim Thaç.; Nexhat Dac.; and Salih Gashi., *Orient. J. Chem.*, **2016**, *32*, 2391-2400.
2. Selvi, S.R.; Baskaran, R.; *Current science.*, **2015**, *109*(7), 1247-1254.
3. Selvi, S.R.; Baskaran, R.; *International journal of engineering science and technology.*, **2015**, *7*(8), 267-278.
4. Selvi, S.R.; Baskaran, R.; *International journal of chem tech research.*, **2014**, *6*(5), 2628-2638.
5. Selvi, S.R.; Baskaran, R.; *International Journal of chem Tech Research.*, **2015**, *8*(11), 211-220.
6. VinodKumar, S.; Baskaran, R.; *IEEE.*, **2019**, *1*, 275-281.
7. VinodKumar, S.; Baskaran, R.; *Studia Rosenthaliana (Journal for the Study of Research).*, **2020**, *XII*(II), 66-71.
8. VinodKumar, S.; Baskaran, R.; *Journal of Xi'an University of Architecture & Technology.*, **2020**, *XII*(III), 5411-5417.
9. VinodKumar, S.; Baskaran, R.; *Journal of Xidian University.*, **2020**, *14*(4), 696-701.
10. VinodKumar, S.; Baskaran, R.; *International J. Advan. Scie. Tech.*, **2020**, *29*, 4450-4454.